

1 Simultaneous CO₂ and CO methanation using microbes

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11 **ABSTRACT**

12 In this study, we developed a method for simultaneous bio-methanation of CO₂ and CO with H₂
13 in a single bioreactor using a combination of carboxydrotrophic bacteria and methanogenic
14 archaea for industrial applications. Methanogenic archaea generally use H₂ and CO₂ to produce
15 methane, whereas very few methanogenic archaea methanize CO, and these grow slowly and
16 consequently produce low reactant gas turnover rates. Thus, to achieve fast and simultaneous
17 transformation of CO and CO₂, we identified a combination of carboxydrotrophic and
18 hydrogenogenic bacteria and methanogenic archaea that can produce H₂ and CO₂ from CO, and
19 then methanize CO₂ and H₂. The present screening experiments identified carboxydrotrophic
20 bacteria and methanogenic archaea that can cohabitate at the same thermophilic temperature and
21 pH ranges and in the same growth medium. In these experiments, combinations of
22 *Carboxydocella thermautotrophica* (DSM 12326), *Carboxydocella sporoproducens* (DSM
23 16521), and three thermophilic rod-shaped methanogenic archaeal cultures from MicroPyros
24 GmbH formed unique microbial co-cultures that transformed CO₂, H₂, and CO to methane. The
25 successful combination of these microbes could be used to gasify biowastes, such as sewage
26 sludge, as alternative sources of hydrogen for microbial power-to-gas processes. Accordingly,
27 gasification under these conditions produced H₂-rich gas containing CO₂ and CO, theoretically
28 allowing various types of biowastes to be converted to biomethane, which is CO₂-neutral,
29 storable, and widely applicable as an energy source.

30

31 **IMPORTANCE:**

32 In this study, we hypothesized that the simultaneous bio-methanation of CO₂ and CO with H₂ in a
33 single bioreactor can support the Power-to-Gas technology, a storage technology for renewable

34 energies. We formed a novel co-culture tool that efficiently achieved the fast and simultaneous
35 transformation of CO and CO₂. That novel co-culture consists of *Caroxydocella*
36 *thermautotrophica* (DSM 12326), *C. sporoproducens* (DSM 16521), and three thermophilic rod-
37 shaped methanogenic archaeal cultures from MicroPyros GmbH.

38 **Introduction**

39

40 We hypothesized that the efficient catalysis of the methanation of CO₂ and CO in a single
41 bioreactor can aid in promoting the expansion of renewable energy sources to slow climate
42 change. For the efficient catalysis, we have developed a combination of carboxydrotrophic
43 bacteria and methanogenic archaea.

44 Power-to-Gas (PtG) storage technologies have been developed to support the use of renewable
45 energies, and these use electrical power from renewable sources to split water and generate
46 hydrogen and oxygen. Hydrogen from such hydrolysis reactions can be stored as methane
47 following reactions with CO₂ as follows: $4 \text{H}_2 + \text{CO}_2 \rightarrow \text{CH}_4 + 2 \text{H}_2\text{O}$. Hence, catalysis of such
48 reactions by methanogenic archaea will constitute a microbial PtG technology.

49 The workload and profitability of PtG technologies can be increased using alternative sources of
50 hydrogen when electrical power for hydrogen production is expensive. To this end, gasification
51 of sewerage sludge may provide an adjustable, ecological, and economically rational alternative
52 H₂ source for microbial PtG processes (1), (2). The ensuing gasification produces H₂-rich gas that
53 also contains CO₂ and CO, and could be used directly as a gas mixture for the PtG processes,
54 pending on the methanation of CO.

55 In contrast with chemical-catalyzed synthesis of methane from H₂ and CO₂ using the so-called
56 Sabatier process, microorganism biocatalysts can adapt to gas pollution, are robust to fluctuations
57 of gas contents, and can work at lower temperatures and pressures (3). Multiple methanogenic
58 archaea have been shown to methanize CO₂ and H₂, although very few reportedly methanize CO
59 (4), (5), (6), (7), and these grow slowly and produce low rates of reactant gas turnover (8).
60 However, efficient CO-oxidizing, H₂-producing bacteria have been identified, and these use CO
61 as their only source of carbon and energy (9).

62 Klasson *et al.* (10) previously reported the use of a single co-culture comprising *Rhodospirillum*
63 *rubrum* to convert CO and H₂ to methane and *Methanobacterium*
64 *formicicum* and *Methanosarcina barkeri* to convert H₂ and CO₂ to methane at 34°C. Herein, we
65 identified microbes that could simultaneously methanize CO₂, H₂, and CO at thermophilic growth
66 temperatures. We then devised a novel combination of CO-utilizing and H₂-producing bacteria
67 (CO + H₂O → CO₂ + H₂) with methanogenic archaea (CO₂ + 4 H₂ → CH₄ + 2 H₂O) and showed
68 optimal growth at around 63°C.

69 Our data demonstrate a highly efficient microbial co-culture that transforms CO₂, H₂, and CO to
70 methane. This co-culture comprised a combination of *Carboxydocella thermautotrophica* (DSM
71 12326), *Carboxydocella sporoproducens* (DSM 16521), and three methanogenic archaea cultures
72 from MicroPyros GmbH. The present innovation may provide the basis for gasification of
73 sewage sludge as an alternative source of hydrogen for industrial scale microbial PtG processes.

74 **Materials and Methods**

75 Based on the methods reported by Hofbauer *et al.* (11), we used the synthetic steam gasifier and
76 synthetic air gasifier gas compositions shown in Table 1. Gases were purchased from Tyczka
77 Industrie-Gase of Mannheim, Germany.

78 The present co-cultures were established as combinations of *Carboxydocella thermautotrophica*
79 (DSM 12326; 12), *Carboxydocella sporoproducens* (DSM 16521; 13; so-called Carbos) from
80 Deutsche Sammlung für Mikroorganismen und Zellkulturen of Brunswick, Germany, and a cell
81 mixture of three thermophilic rod-shaped methanogenic archaeal cultures (TRMC) that were
82 kindly supplied by MicroPyros GmbH of Straubing, Germany. TRMC are autotrophic isolates
83 from the biogas plant of Zweckverband Abfallwirtschaft of Straubing, Germany and were
84 selected in screens for reproducible growth in newly designed medium (see below) with synthetic
85 steam gasifier gas and synthetic air gasifier gas. The present isolates showed the best and most
86 reproducible growth among all strains tested and were selected from the MicroPyros culture
87 collection. *Carboxydocella sporoproducens* cells grow more slowly than *Carboxydocella*
88 *thermautotrophica* cells but can form stable spores that survive periods of CO
89 deprivation (12), (13). To ensure sustained supply, cultures were transferred into fresh media
90 weekly (5% inoculation) and were incubated at 63°C for 24 h. All experiments were performed in
91 triplicate for at least five transfers.

92 Growth media were prepared as described by Zhao *et al.* (14), except that the expensive vitamin
93 and yeast extract supplements were omitted for future industrial scale-up. The final media
94 contained (g/L) KCl (0.33), MgCl₂×6H₂O (0.102), CaCl₂×2H₂O (0.015), NH₄Cl (0.33), K₂HPO₄
95 (0.14), and NaHCO₃ (0.42) in demineralized water. A trace element solution (10 mL/L) and a

96 selenite-tungstate solution (0.1 mL/L) were added as described for DSMZ medium 14 and DSMZ
97 medium 385.

98 Oxygen was expelled from media solutions using the argon method described by Hungate (15)
99 with minor modifications. Subsequently, 0.7 g/L of Na₂S×9H₂O was added, and media were
100 introduced to anaerobic chambers and were dispensed into 28 mL serum tubes at 5 mL per tube.
101 Tubes were then sealed with rubber stoppers and were pressurized to 3 bar absolute using the
102 desired gas phase. Gas phases in glass tubes were then exchanged by degassing and gassing three
103 times. Pressurized tubes were then autoclaved at 121°C for 15 min (15), (16) and the pH of the
104 autoclaved medium was about 6.5. Culture tubes were incubated almost horizontally to maximize
105 contact areas of gas and liquid phases, and gases entered liquid phases containing
106 microorganisms solely by diffusion. Samples of cultures were taken using syringes (Omnifix-
107 F®), and numbers of cells were counted using fluorescence microscopy (Olympus BX53F) with
108 a Thoma counting chamber. Numbers of cells in TRMC were determined by counting fluorescent
109 cells, and pH was determined using pH sticks (pH-Fix; 4.5–10.0, Roth). Pressure levels in culture
110 tubes were determined using a portable WAL 0–4 bar absolute membrane pressure unit (Wal
111 Mess- und Regelsysteme GmbH of Oldenburg, Germany).

112 H₂, CO, CO₂, CH₄, and N₂ contents were quantified using a Thermo Fisher Scientific Trace 1310
113 gas chromatograph with a thermal conductivity detector. In these determinations, 400 µL aliquots
114 of gas were taken from the headspaces of culture tubes and were added to a packed Supelco
115 Carboxen-1000 column (Gas Syringe A-2, Macherey-Nagel of Düren, Germany). The column
116 was then heated to 108°C and maintained at this temperature for 6.25 min, followed by heating to
117 177°C at 120°C/min and maintenance at this temperature for 3.2 min. Finally, the column was
118 heated at 120°C/min to 222°C and was maintained at this temperature for 4.6 min. Argon was

119 used as the carrier gas at a flow rate of 11 mL/min. The injector and detector were adjusted to
120 125°C and 235°C, respectively. Measured GC values were standardized to 100%. Finally,
121 methane production rates (MPR) were calculated as ml of CH₄ produced/(mL medium *h).

122 **Results**

123 **Co-culture**

124 *Carboxydocella thermautotrophica*, *Carboxydocella sporoprducens* (Carbos), and cells from the
125 three thermophilic rod-shaped methanogenic archaeal isolates (TRMC) proliferated well together
126 in the newly designed medium without vitamin solution or yeast extract and under the growth
127 conditions are presented in Table 2 (11), (12).

128

129

130 **Metabolic properties of TRMC isolates**

131 Mixtures of the three methanogenic archaeal isolates methanated CO₂ and consumed H₂ from the
132 gas phase in the volumes shown in Fig. 1. However, CO conversion was not observed with either
133 steam gasifier or air gasifier gas (Fig. 1).

134

135 Fig. 1: Gas compositions at 0 and 71.3-h incubation of TMRC in air gasifier gas

136

137 **Growth experiments with Carbos and TRMC**

138 In initial experiments with combinations of Carbos and TRMC, microscope analyses showed the
139 presence of fluorescent methanogenic archaea and the morphologically shorter non-fluorescent
140 carboxydrotrophic, hydrogenogenic bacteria growing in co-culture (Fig. 2), with an estimated
141 TRMC to Carbos ratio of about 2:1 (Fig. 2).

142
143 Fig. 2: Co-culture of methanogenic archaea (TRMC; blue-colored rods) with carboxydrotrophic
144 bacteria (Carbos; black-colored rods) in steam gasifier gas after 96 h incubation at 63°C

145
146 **Consumption of steam gasifier gas by co-cultures**

147 Figure 3 shows simultaneous decreases in H₂ and CO concentrations and concomitant increases
148 in CH₄ contents of the gas phase. In these experiments, calculated maximum methane
149 concentrations in the headspace were achieved within 96 h, based on reaction equations CO +
150 H₂O → H₂ + CO₂ [1] and CO₂ + 4 H₂ → CH₄ + 2 H₂O [2]. Moreover, CO₂ concentrations were
151 increased immediately and then remained approximately constant, and pressure (p) profiles (p
152 actual / p start) dropped during methanation to about 44% of the initial pressure.

153
154 Fig. 3: Changes in gas compositions and pressure during incubation in steam gasifier gas; error
155 bars indicate standard deviations of three measurements

156

157 Initial hydrogen concentrations were 50% and dropped to 0.5% within 72 h, and CO
158 concentrations decreased from 20% to 3% over the same time. Concomitantly, methane
159 concentrations increased from 10% to 53%, and after 96 h incubation, H₂ concentrations were
160 0%, CO concentrations were 2%, and methane concentrations were 55% of the entire volume.
161 Moreover, increases in methane concentrations increased by about 1.0 vol%/h between 24 and 48
162 h, corresponding with a methane production rate of 0.03 mL/(mL*h).

163 The maximum possible methane concentration in the steam gasifier gas phase following
164 complete H₂ and CO methanation according to equations [1] and [2] was 55 vol%, and the total
165 methane production rate from 10 vol% to 55 vol% methane over the entire 96 h incubation time
166 was 0.02 mL/(mL*h).

167 During growth experiments in steam gasifier gas, numbers of cells in Carbos and TRMC
168 increased during the first period of methanation, and then decreased and remained stable at about
169 1×10^8 cells/mL (Fig. 4).

170 Fig. 4: Changes in cell numbers over the incubation period in steam gasifier gas at 63°C; standard
171 deviations of three measurements are indicated by error bars

172 **Consumption of air gasifier gas by co-cultures**

173
174 H₂ and CO contents decreased with increases in CH₄ concentrations in the gas phase (Figure 5),
175 and the calculated maximum methane concentration in the headspace was achieved within 72 h.
176 Simultaneously, pressure profiles in the gas phase of the glass tubes ($p_{\text{actual}} / p_{\text{start}}$) dropped to
177 about 69% of the initial pressure during methanation. In accordance, hydrogen concentrations in
178 air gasifier gas dropped from 15% to 1.5% over 48 h. Concomitantly, CO concentrations

179 decreased from 20% to 3%, and methane concentrations increased from 10% to 21%. After 96 h,
180 the hydrogen concentration was 0%, the CO concentration was 1%, and the methane
181 concentration was 22% of the total volume, and this concentration was maximal in air gasifier
182 gas following complete H₂ and CO methanation, according to equations [1] and [2]. Moreover, in
183 calculations of MPR, methane concentrations increased by 0.22 vol%/h between 24 and 48 h
184 incubation, corresponding with a production rate of 0.01 mL/(mL*h). Similarly, the total methane
185 production rate from 10 vol% methane at 0 h to 22 vol% at 72 h was 0.01 mL/(mL*h).

186

187 Fig. 5: Changes in gas composition and pressure over the incubation period in air gasifier gas;
188 standard deviations of three measurements are indicated by error bars

189

190 Growth experiments in air gasifier gas showed initial increases in cell numbers in Carbos and
191 TRMC, followed by decreases to 0.5×10^8 /mL and 0.8×10^8 /mL, respectively (Fig. 6).

192

193 Fig. 6: Changes cell numbers over the incubation period in air gasifier gas; standard deviations of
194 three measurements are indicated by error bars

195

196 **Discussion**

197 In the present novel combination cultures of thermophilic methanogenic archaea and
198 thermophilic carboxydophilic and hydrogenogenic bacteria, growth of all three organisms in

199 synthetic steam gasifier gas and in synthetic air gasifier gas was observed, and CO, CO₂, and H₂
200 were converted into methane. In addition, the ensuing increases in methane concentrations
201 corresponded with the stoichiometric ratios indicated by the equations $\text{CO} + \text{H}_2\text{O} \rightarrow \text{H}_2 + \text{CO}_2$
202 and $\text{CO}_2 + 4 \text{H}_2 \rightarrow \text{CH}_4 + 2 \text{H}_2\text{O}$.

203 Consistent with kinetic expectations, methane production slowed with decreasing reactant gas
204 concentrations and lower pressures in culture tubes, reflecting decreased substrate gas
205 availability. However, in air gasifier gas, methanation proceeded more slowly due to lower
206 hydrogen partial pressures compared with those in steam gasifier gas. Klasson *et al.* previously
207 showed simultaneous conversion of the gases CO and H₂ by *Rhodospirillum rubrum* and H₂ and
208 CO₂ by *Methanobacterium formicicum* and *Methanosarcina barkeri* in growing co-cultures at
209 34°C. In their study, *R. rubrum* growth was dependent on the presence of tungsten, light, and a
210 carbon source other than CO, such as sugars, acetate, or yeast extract, and vitamin supplements
211 were also provided (10), (17). In contrast, the present unique microbial combination grew
212 optimally at 63°C and remained viable in the absence of light and expensive vitamin supplements
213 and carbon sources, thus increasing the convenience and cost-effectiveness of large-scale
214 cultures. Moreover, in the study by Klasson *et al.*, methane yields from H₂ were 83% of the
215 theoretical maximal yield (10), whereas we achieved 100% of theoretical maximal methane
216 concentrations in the gas phase using synthetic steam and air gasifier gases. As a final advantage,
217 the present co-culture system with spore-forming *Carboxydocella sporoproducens* was robust to
218 periods of CO deficiency.

219 In summary, we demonstrated the use of a novel co-culture tool that efficiently allows the use of
220 biowastes as sources of carbon and energy using gasification followed by biological methanation.
221 This novel technology could also be applied to other CO₂, H₂, and CO-containing gases, such as

222 exhaust gases from steel production, allowing use as raw materials for the production of CO₂-
223 neutral methane in industrial processes (18).

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274

275 **Figure Legends**

276 Fig. 1: Gas compositions at 0 and 71.3-h incubation of TMRC in air gasifier gas

277 Fig. 2: Co-culture of methanogenic archaea (TRMC; blue-colored rods) with carboxydophilic
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283 Fig. 5: Changes in gas composition and pressure over the incubation period in air gasifier gas;
284 standard deviations of three measurements are indicated by error bars

285 Fig. 6: Changes cell numbers over the incubation period in air gasifier gas; standard deviations of
286 three measurements are indicated by error bars

287

Table 1 Gas concentrations of steam gasifier and air gasifier gases

	Steam gasifier gas [vol%]	Air gasifier gas [vol%]
H ₂	50	15
CO	20	20
CO ₂	20	20
CH ₄	10	10
N ₂	0	35

Table 2 Growth conditions

Growth conditions	<i>Carboxydocella thermautotrophica</i> (Range; Optimum)	<i>Carboxydocella sporoproducens</i> (Range; Optimum)	TRMC (Culture Conditions: MicroPyros)	Conditions used for the co-culture (This study)
T [°C]	40–68; 58	50–70; 60	63	63
pH	6.5–7.6; 7	6.2–8.0; 6.8	6.5	6.5
Metabolic reaction	$\text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2$	$\text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2$	$\text{CO}_2 + 4\text{H}_2 \rightarrow \text{CH}_4 + 2\text{H}_2\text{O}$	This study











